

# **NO<sub>x</sub> Adsorber Regeneration Phenomena In Heavy Duty Applications**

**ORNL/ITEC CRADA**

**Brian West**

**John Thomas, Mike Kass, John Storey, Sam Lewis**

**Oak Ridge National Laboratory**

**Industrial Partners**

**Xinqun Gui, Shouxian Ren**

**Ken Price, Danan Dou**

**DELPHI**



**2003 Diesel Engine Emissions Reduction Workshop  
August 24-28, 2003**

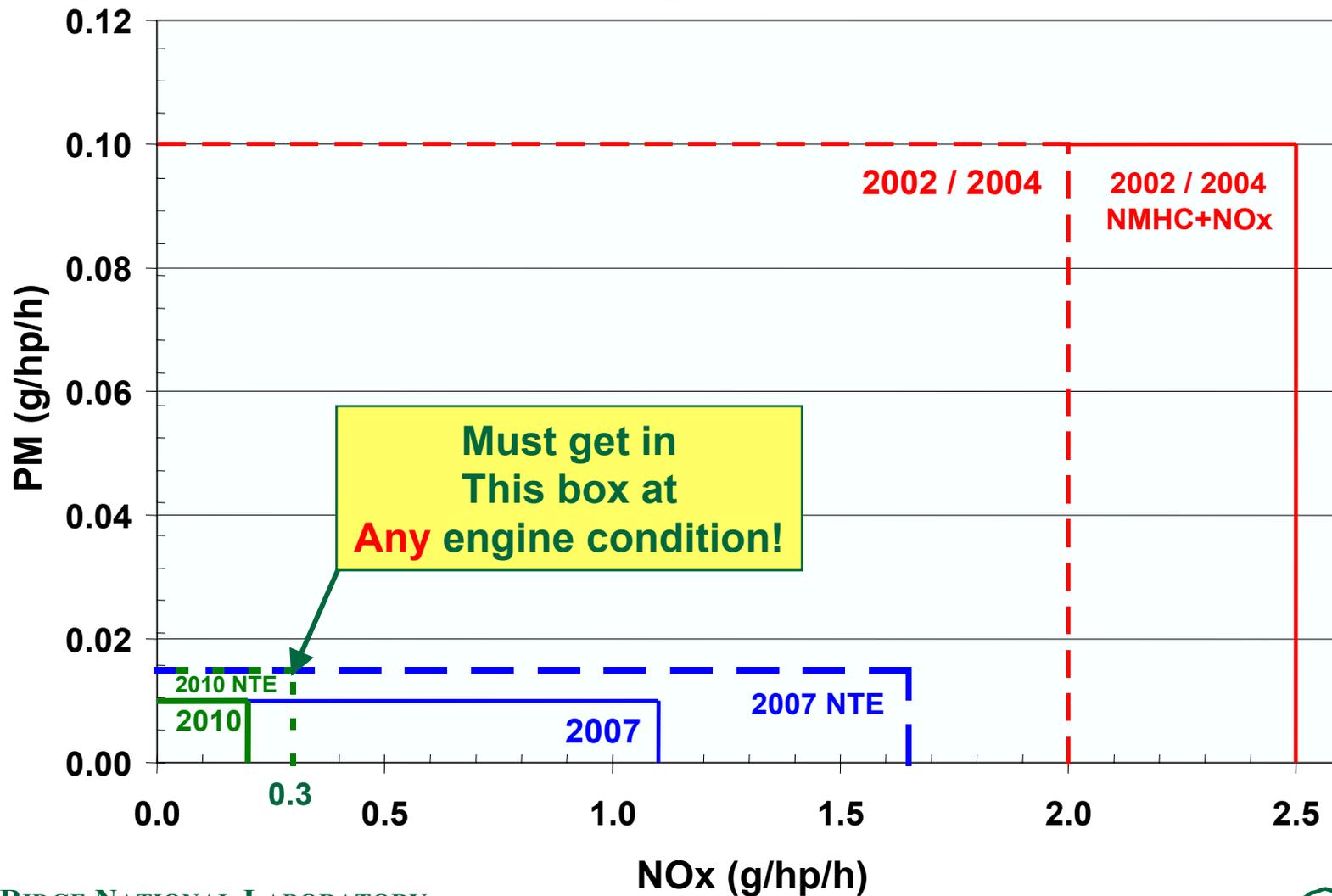
**Sponsor: U.S. Department of Energy, OFCVT**

**Team Leader: Gurpreet Singh**

**OAK RIDGE NATIONAL LABORATORY  
U. S. DEPARTMENT OF ENERGY**

The logo for UT-Battelle, featuring a stylized green mountain range above the text "UT-BATTELLE" which is underlined.

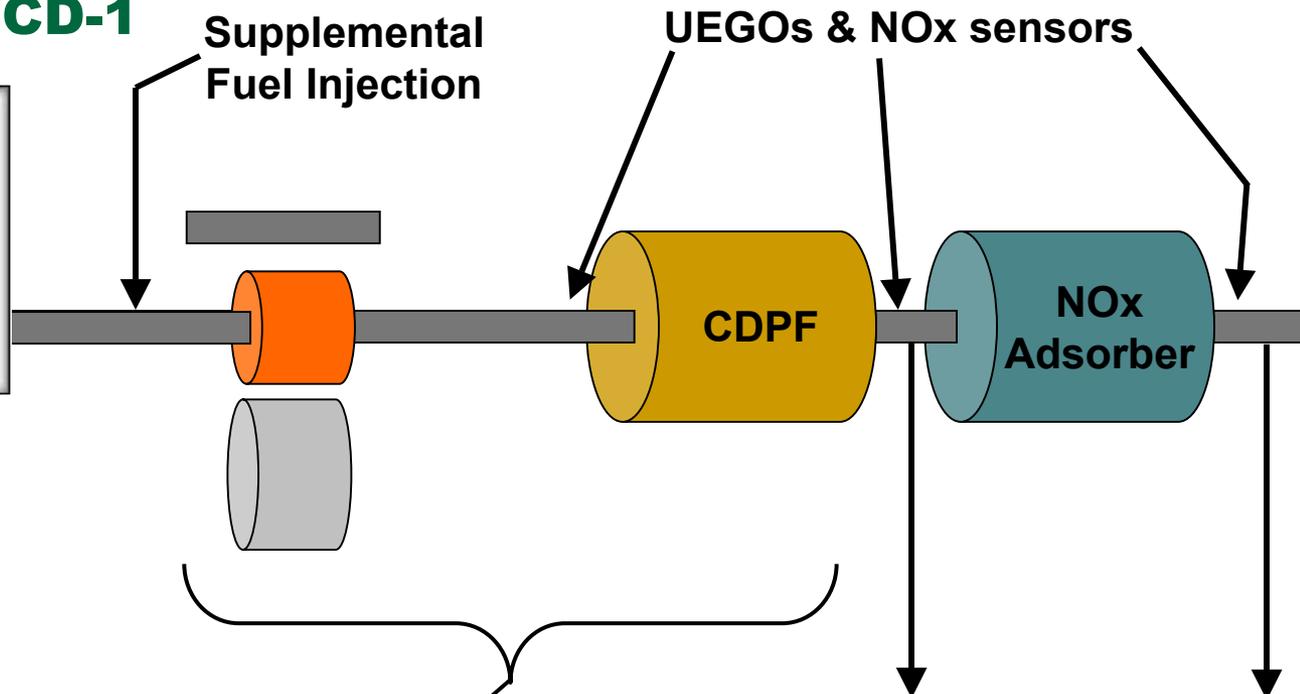
# Impending HD standards call for drastic emissions reductions. NTE limits impose significant challenge



# Diesel oxidation cats inserted downstream of injection site. CDPF and NOx adsorber in all experiments. Unless otherwise specified, test fuel is ECD-1



**T444E Engine**  
w/ Throttle, EGR



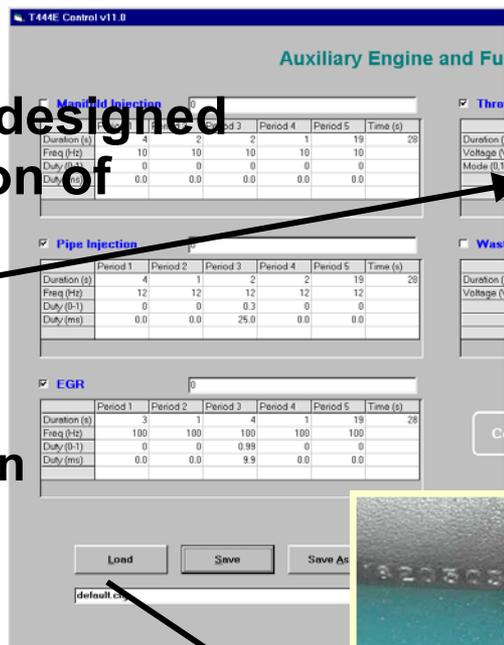
Straight Pipe + CDPF: mild oxidation  
 2.5 L DOC + CDPF: moderate oxidation  
 5 L DOC + CDPF: aggressive oxidation

Samples to microdiluter for  
 FTIR (continuous), GC-MS (bags)

# ITEC T444E Engine modified to control aftertreatment system

## □ PC-based auxiliary controller designed and built for transient operation of

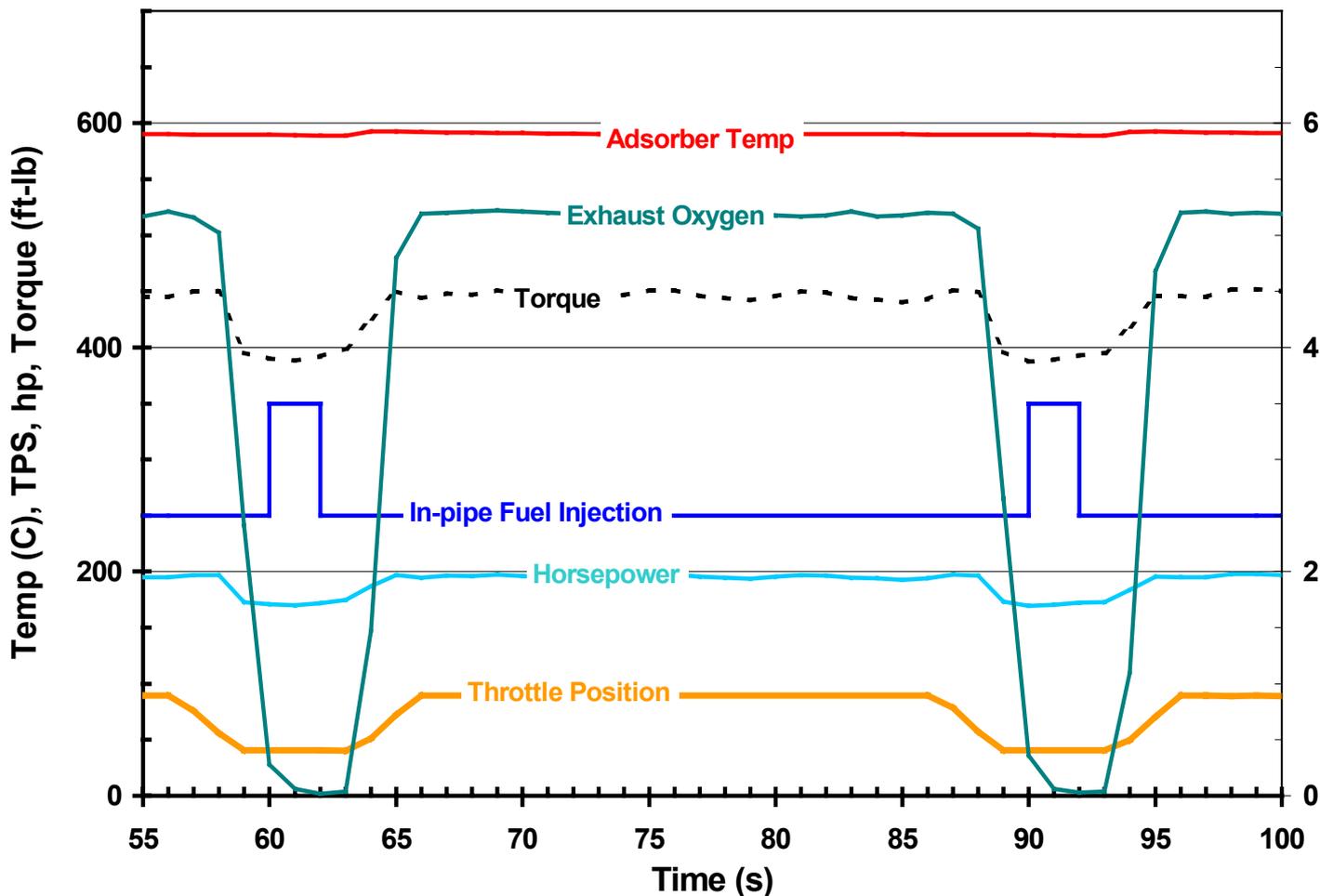
- Electronic throttle
- Electronic EGR valve
- Wastegate
- Post-combustion fuel injection
  - In-manifold (pre-turbo)
  - In-pipe (after turbo)



## □ Aftertreatment system includes diesel oxidation catalyst(s), catalyzed diesel particulate filter, and NOx adsorber



# Sample strategy for regeneration with in-pipe injection



2300 RPM, 450 ft-lb  
Adsorber temperature 600C

30 s cycle time

2 s throttle ramp to 40%, hold 5 s

3 s rich pulse

No attempt to mitigate torque loss

Exhaust O2 %

# All experiments used same NOx adsorber with CDPF upstream. CDPF augmented with DOCs

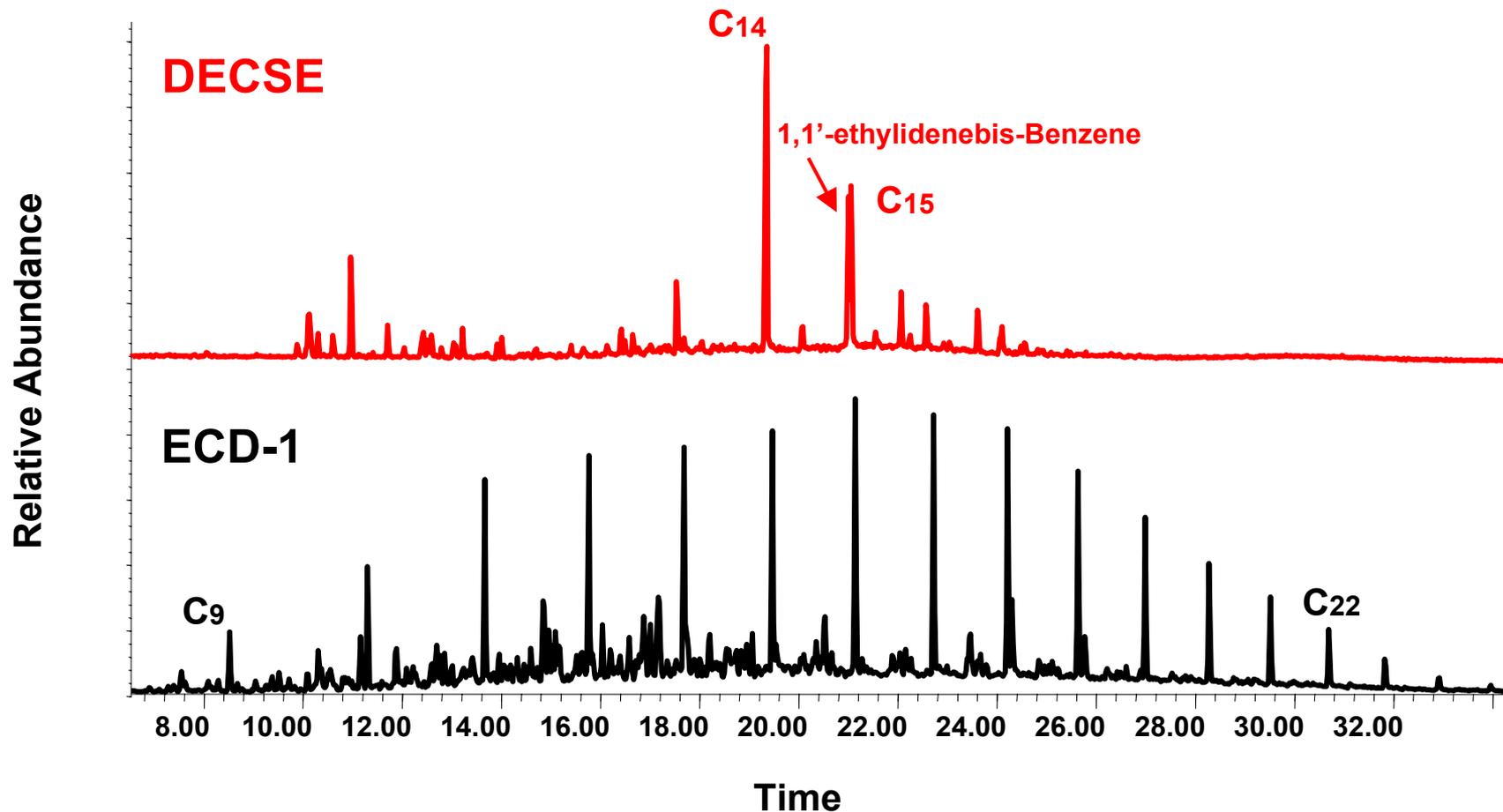
Device	Volume (L)	Min SV (1000/hr) (Regen)	Max SV (1000/hr) (Lean operation)	PGM g/ft <sup>3</sup>
Small DOC	2.5	204	307	70
Large DOC	5	102	154	70
CDPF (not Delphi part)	15	34	51	75
NOx Adsorber (Ba-K type)	14	36	55	100

# **Fuel used in this study is largely BP (Arco) ECD-1. Cursory look at DECSE**

- **EPA's 2006 Diesel Fuel spec differs from today's only in sulfur level**
- **EPA and CARB certification fuel specs differ in aromatics (EPA >27; Cal <10) and cetane**
- **BP (Arco) ECD-1 "looks" like CARB fuel**
- **"DECSE" (Chevron Phillips ULS), BP15, and S-zorb™ "look" like 2006 EPA fuels**
  - **Aromatics, boiling range, sulfur**

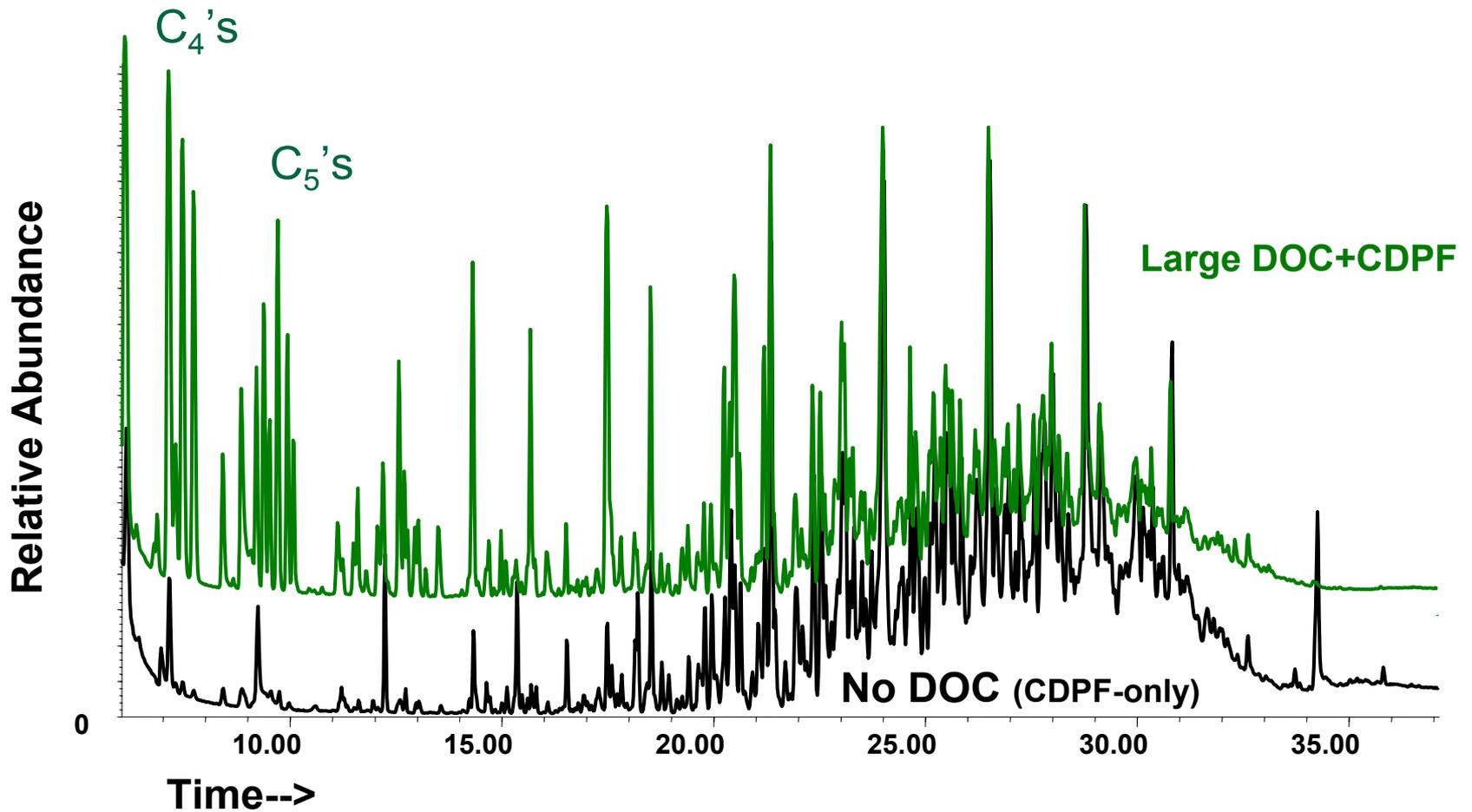
# DECSE fuel meets all specs, but contains narrow range of HCs

Chromatogram shows individual compounds in DECSE and ECD-1 fuel



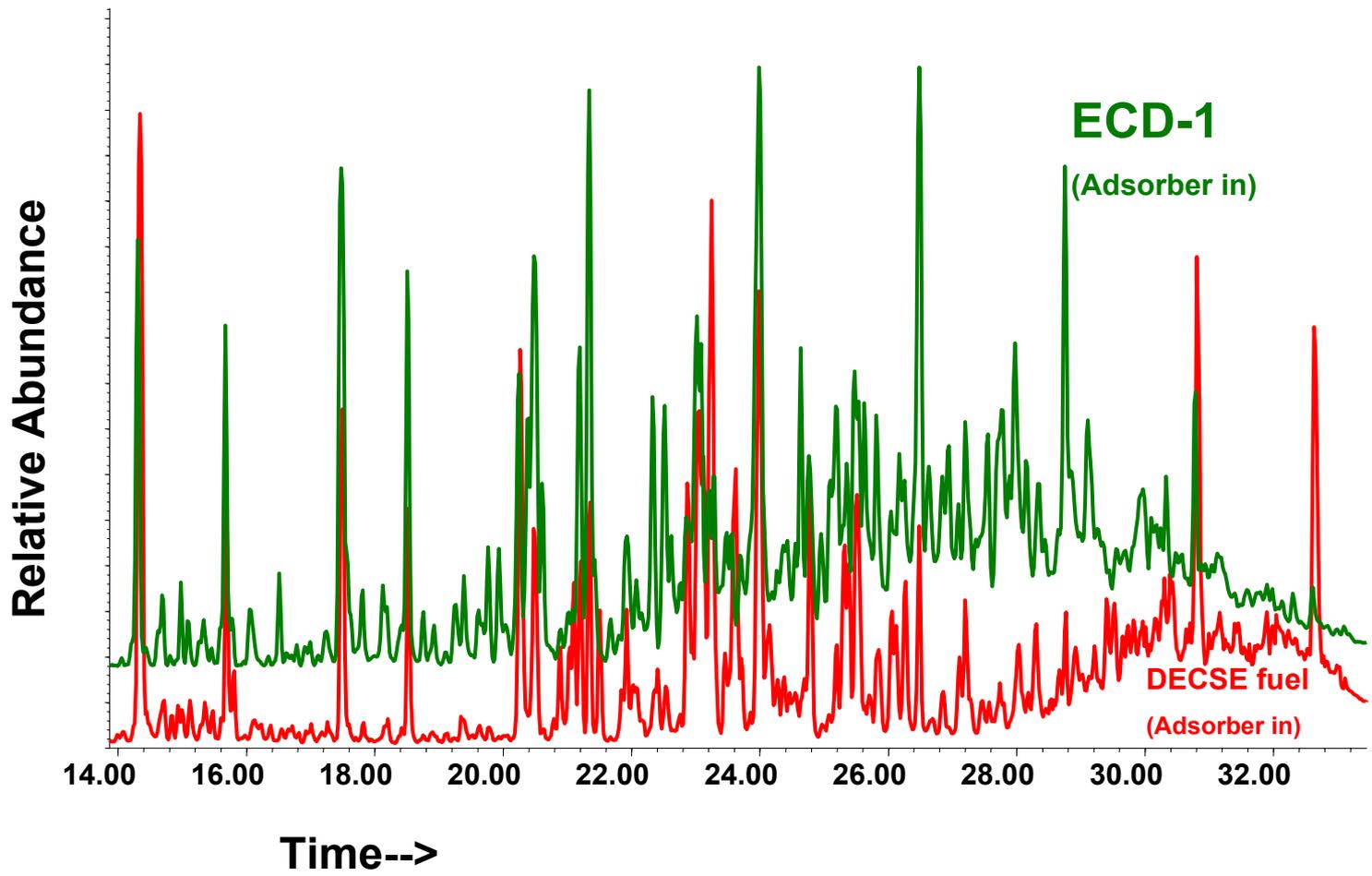
# Large DOC provides extensive HC cracking and lighter HCs to Adsorber

Large DOC vs no DOC, 0.4 DC, ECD-1, Adsorber in



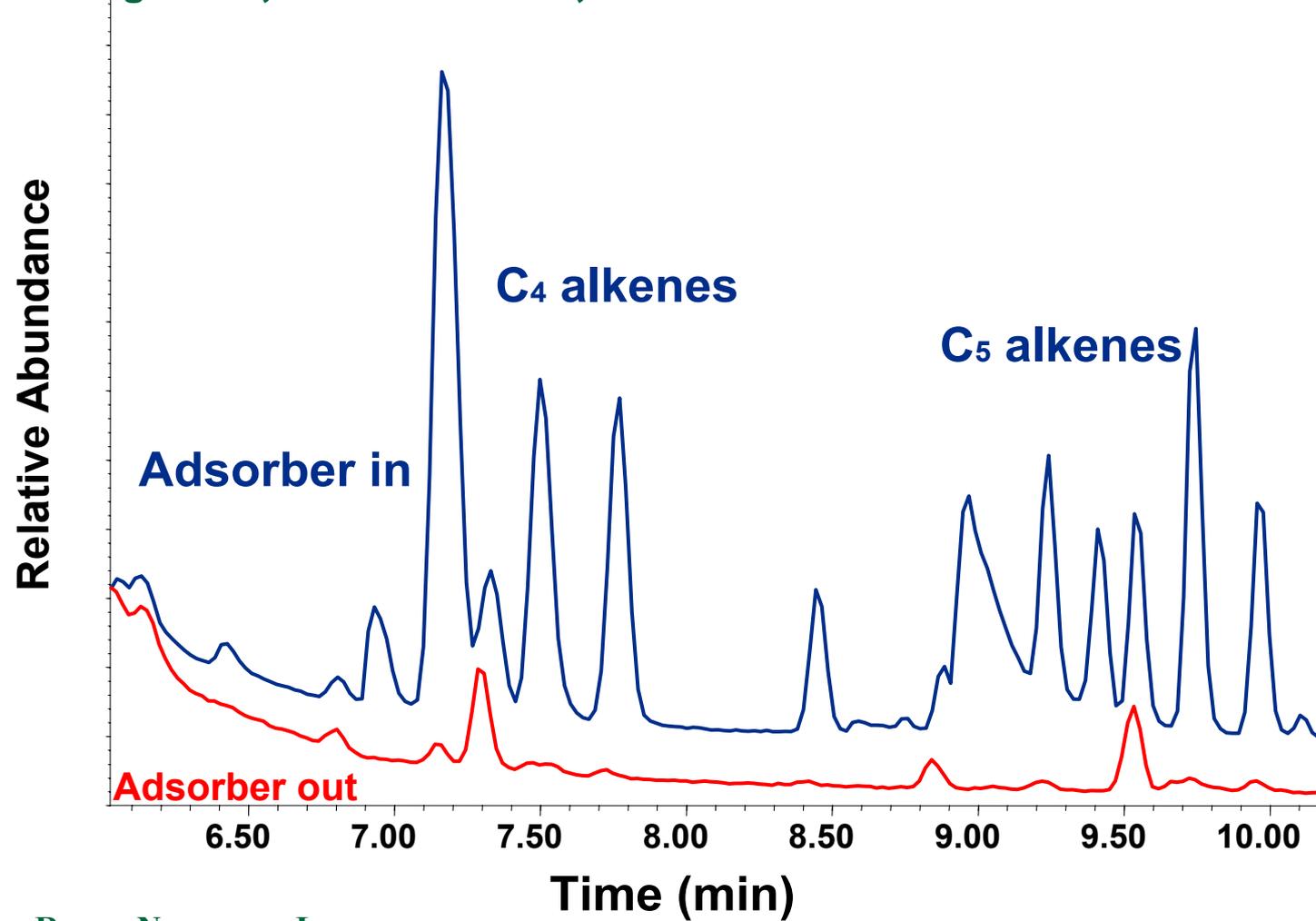
# ECD-1 Fuel yields broader range of HCs at Adsorber inlet than DECSE fuel

Large DOC, 0.4 DC, **DECSE** vs ECD, Adsorber in

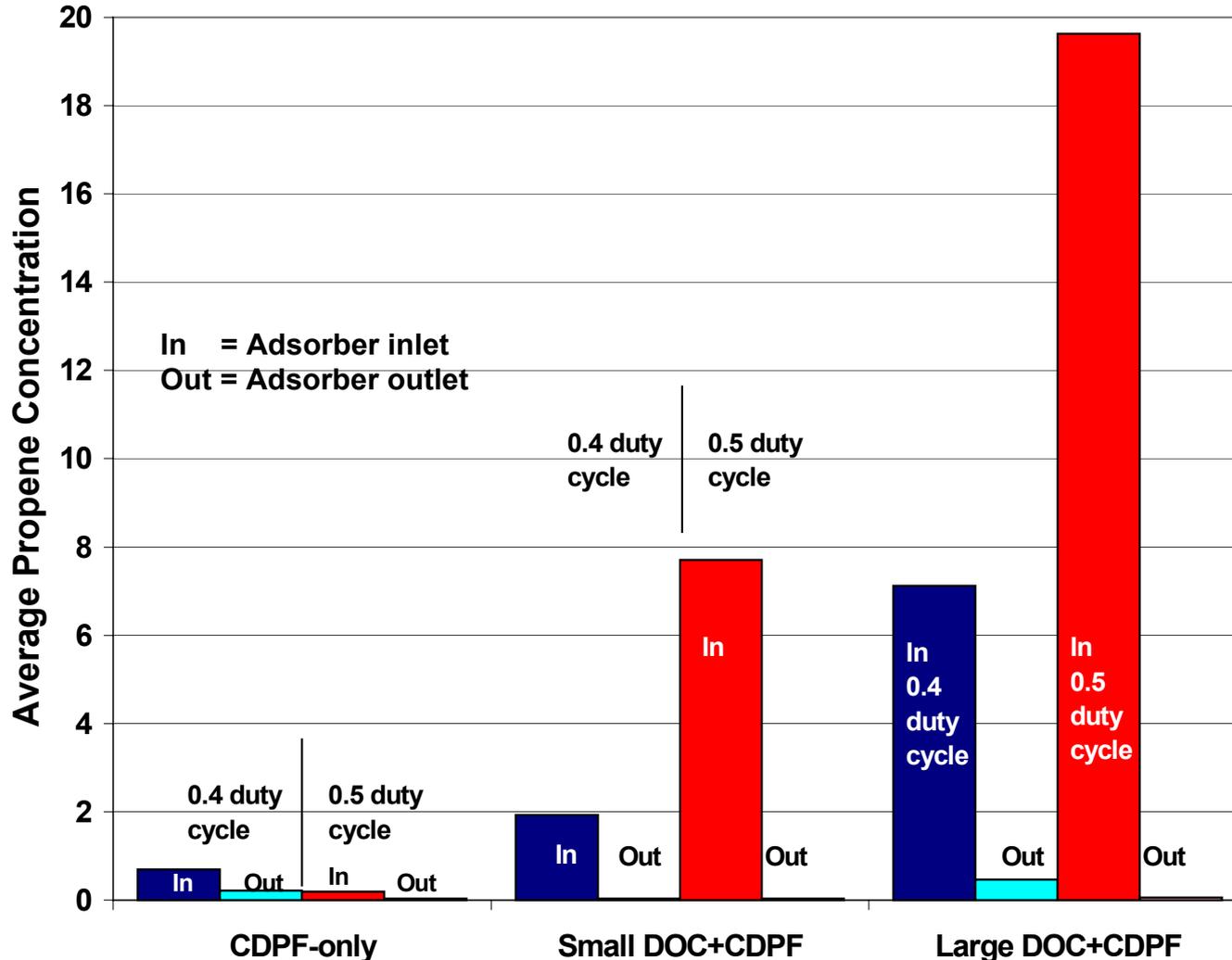


# GC-MS shows C4 and C5 HCs at adsorber inlet, all utilized by NOx adsorber catalyst. Light alkenes are formed in upstream catalysts.

Large DOC, 0.4 DC in vs out, DECSE



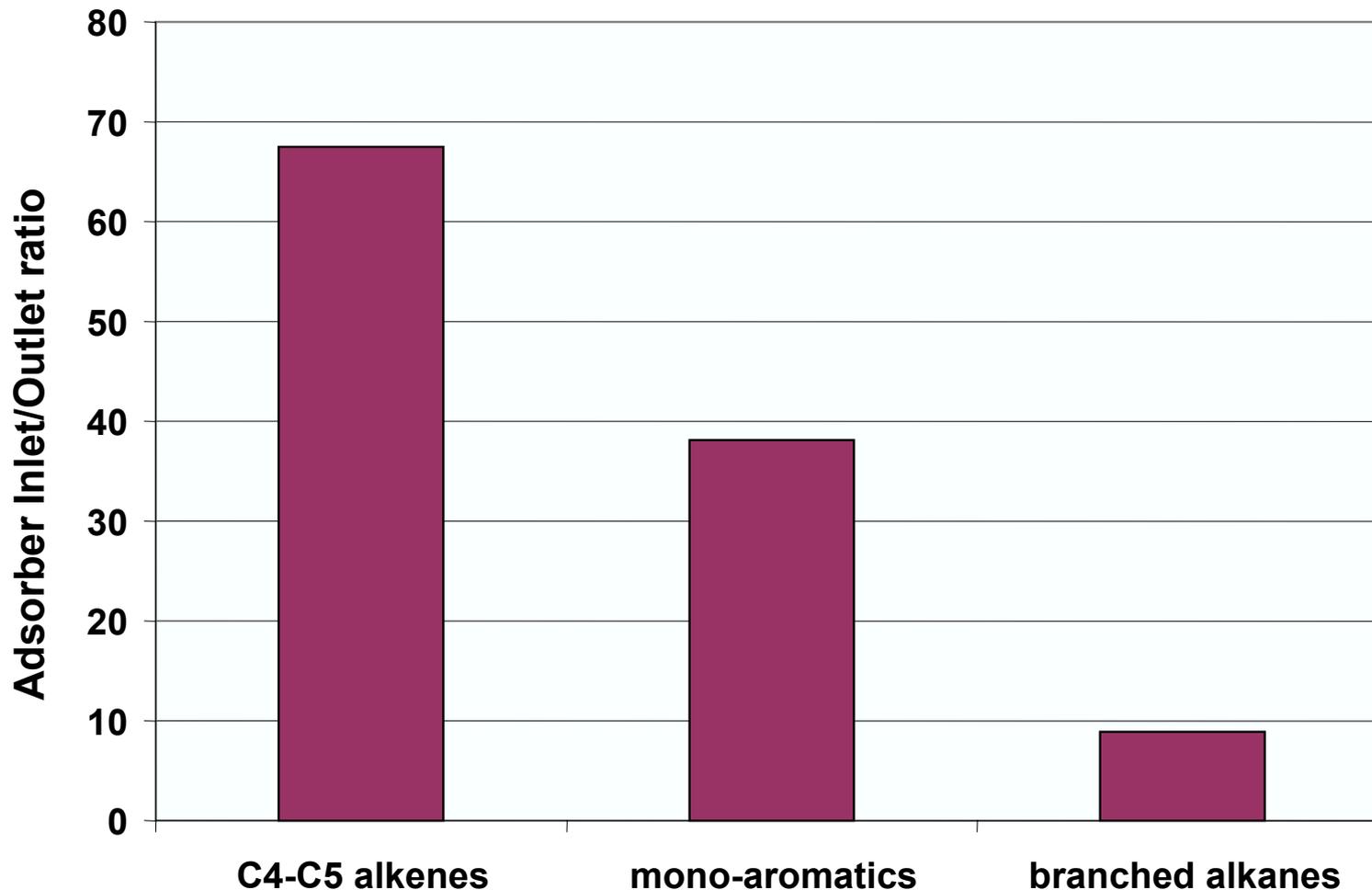
# Oxidation catalysts promote propene formation, readily utilized by NOx adsorber



- Data from FTIR
- Larger diesel oxidation catalyst (DOC) makes most propene
- Richest calibration produces most propene w/ DOC
- Duty cycle is fractional on time for periodic in-pipe injector

# Light alkenes and mono-aromatics are readily utilized by NO<sub>x</sub> adsorber. Branched alkanes are less preferred. Are aromatics good?

Average adsorber inlet/outlet concentration of families of compounds shown for several cases, both ECD-1 and DECSE fuels, with oxidation catalyst and CDPF upstream of NO<sub>x</sub> adsorber.



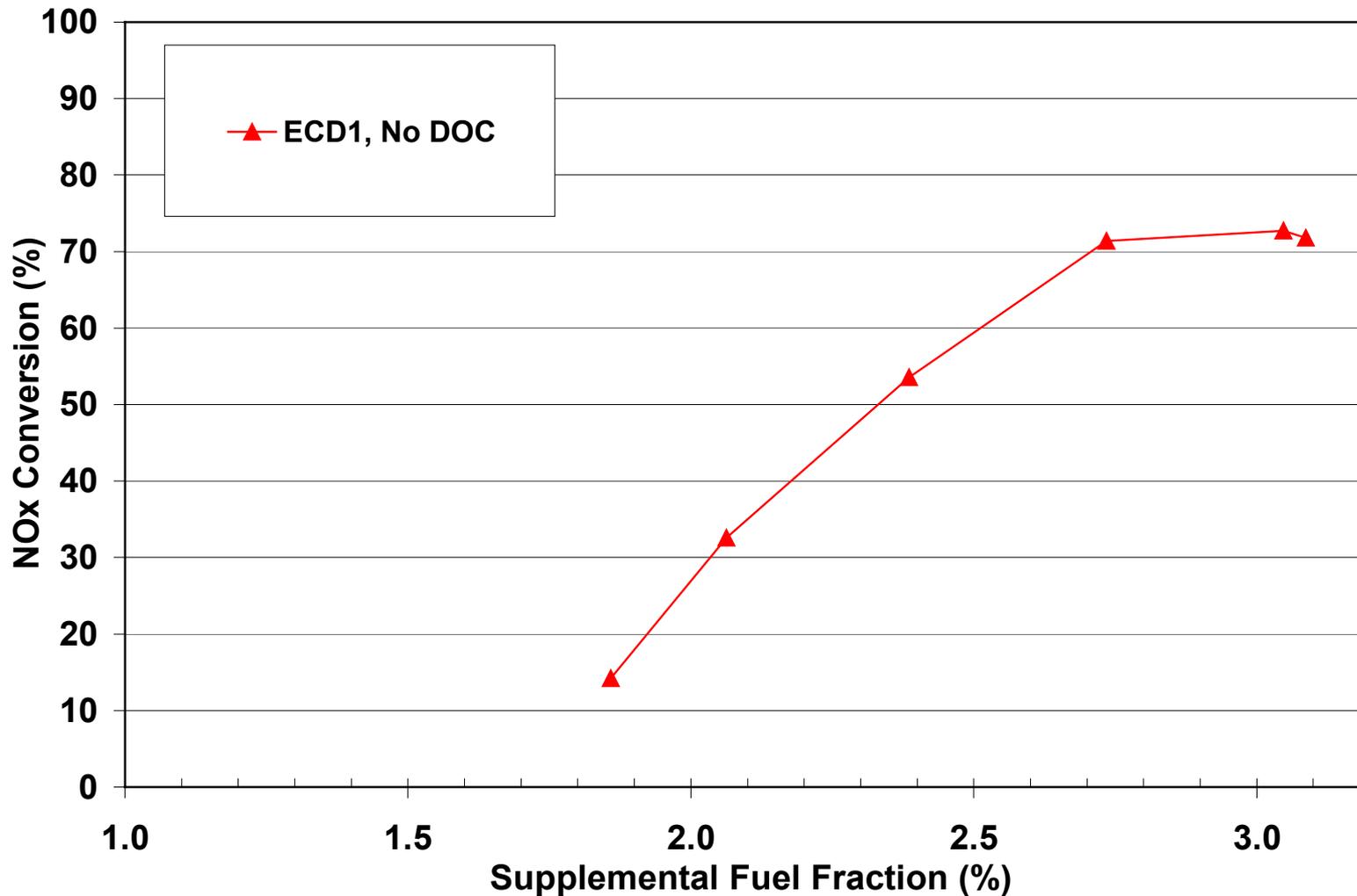
- **Monoaromatics and light alkenes**
  - Formed in exhaust from raw fuel
  - Well utilized by NOx adsorber
  
- **All tailpipe HC emissions are below NTE limit of 0.21 g/hp/hr**

**We have shown that fuel cracking in DOCs provides different species to the NO<sub>x</sub> adsorber.**

**What affect does this have on NO<sub>x</sub> reduction?**

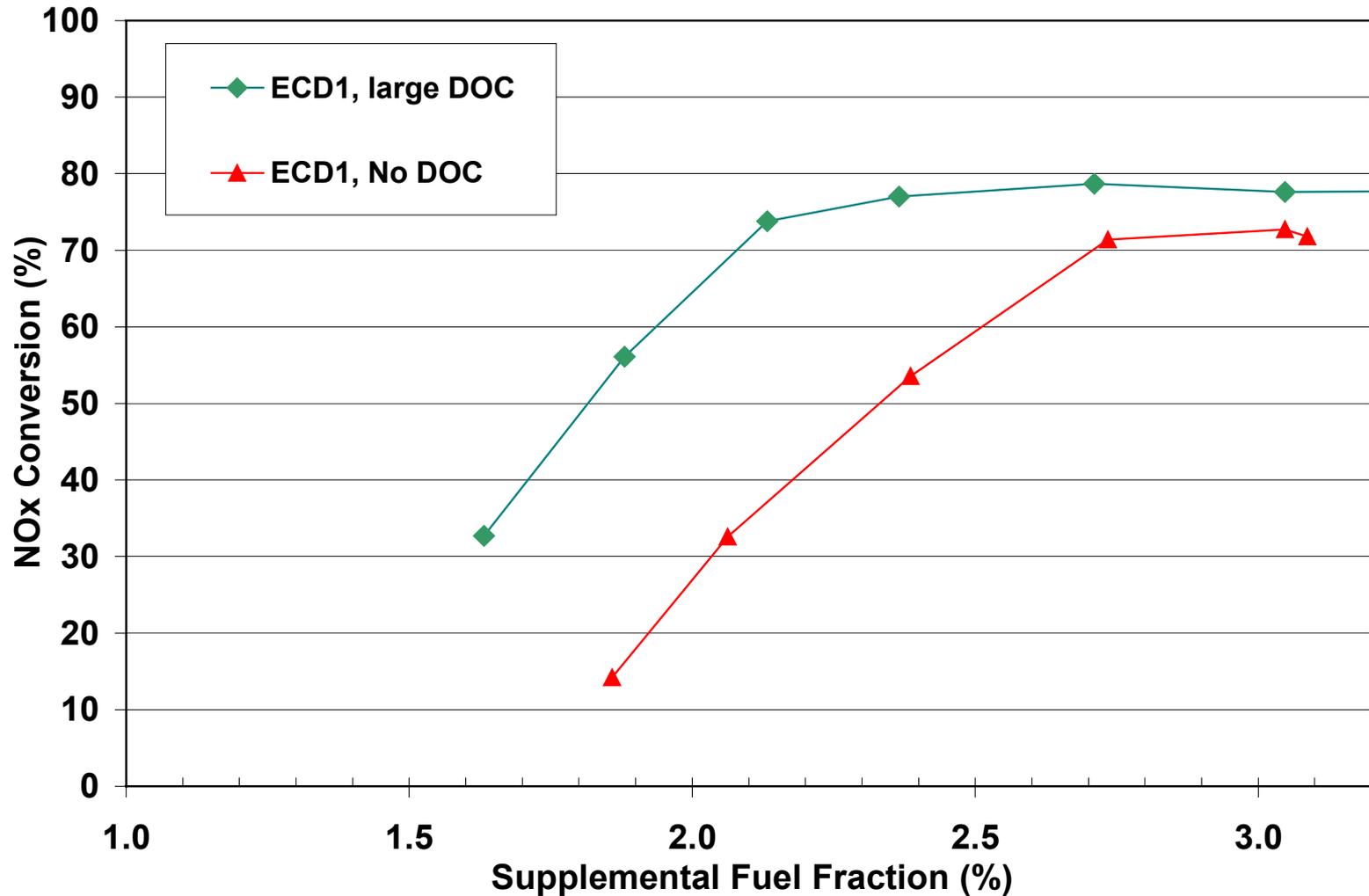
# With no upstream DOC, 70% NOx reduction achieved at ~2.7% excess fuel

Full Load, Rated Speed condition, 600C Catalyst temperature



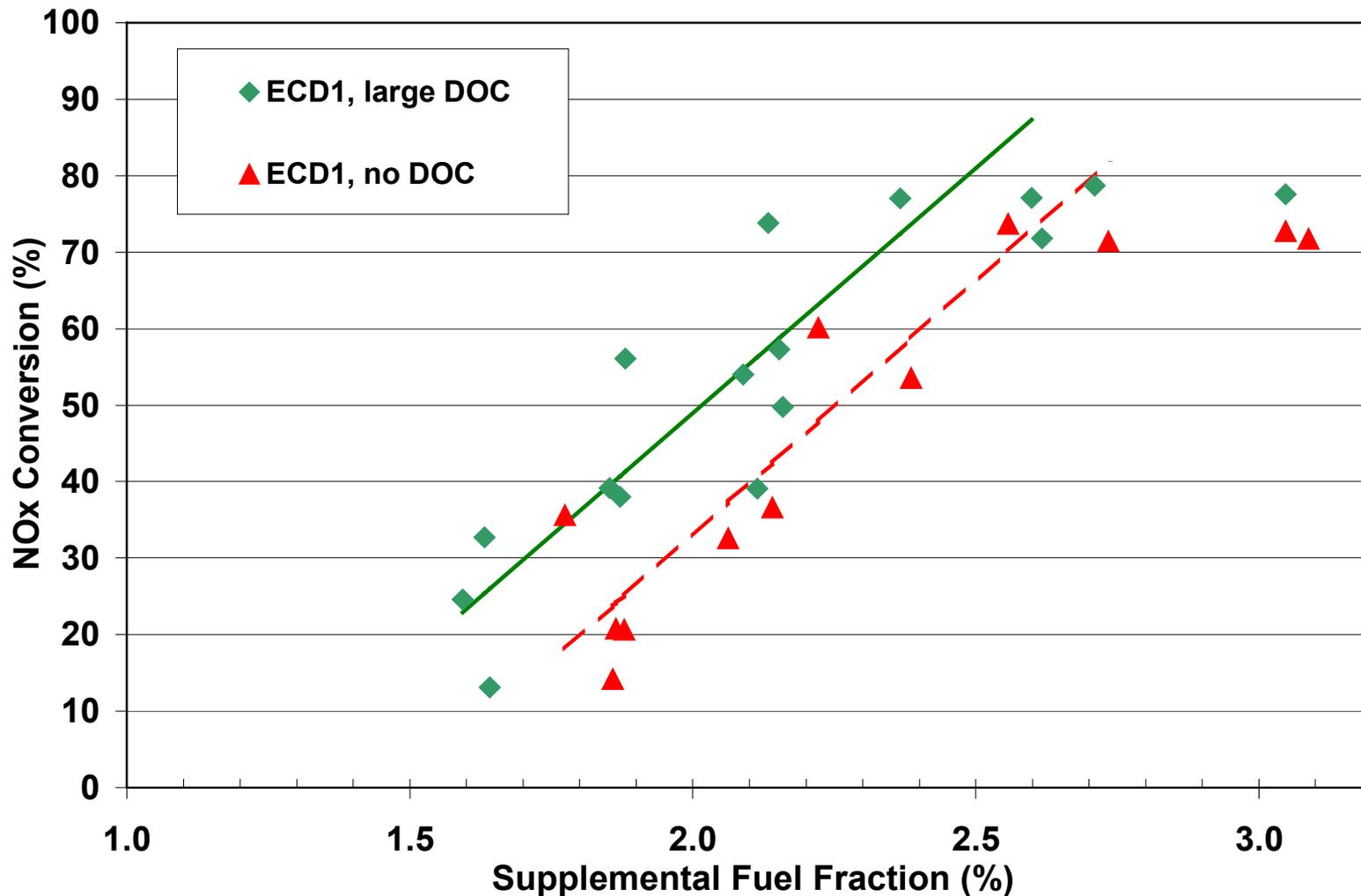
# Fuel cracking in DOC lowers fuel penalty for equivalent NOx reduction

Full Load, Rated Speed condition, 600C Catalyst temperature



# Data from multiple runs shows consistent 10% reduction in fuel penalty with DOC

Full Load, Rated Speed condition, 600C Catalyst temperature



# Summary and Conclusions-1

- **Light alkenes, mono-aromatics preferred by NO<sub>x</sub> adsorber**
  - Branched alkanes not as good
  - Suspect an increase in HC sensitivity at lower temperatures (we were at 600°C)
  - Understanding preferred HC species may help choose “best” certification fuel
    - Many “clean” diesel fuels are low aromatic

# Summary and Conclusions-2

- ~70% NO<sub>x</sub> reduction achieved at 600 °C NTE condition
  - Caveats:
    - Large, “young” catalyst (150-200 hours)
      - Negligible sulfur poisoning, no desulfations as yet
    - High engine-out NO<sub>x</sub> (~5 g/hp/hr)
    - Only 2 - 2.5% excess fuel
  - 70% NO<sub>x</sub> reduction will require <1.0 g NO<sub>x</sub>/hp/hr **engine-out** in 2010 to meet NTE
  - 2.0 g NO<sub>x</sub>/hp/hr engine-out will require **>85%** reduction
    - Larger/improved adsorber, more frequent regen, best reductant
- NTE imposes *significant* challenge

# Acknowledgments

- **Program sponsors:**

Gurpreet Singh, Kevin Stork, OFCVT



- **Industrial Partners:**

Xinqun Gui, Shouxian Ren



Ken Price, Danan Dou

**DELPHI**